

## Supplemental Problem A-6

Ch. 12 Materials Handling

**Goal:** Determine total installed cost of pump & piping system

**Given:** Water pipe 275 gpm 75 F 1000 feet  
 delivery rate water temperature length 304.8 meter length  
 black carbon steel Insulation, 85% magnesia 1.5 inch thickness  
 Fittings 40 Valves 4  
 Pump 10 hp centrifugal  
 Motor AC enclosed 3-phase 1800 rpm

**Approach:** Determine optimum pipe diameter, use eqn. 12-15 or Fig. 12-3

$$D_{i,opt} = 0.363 m_v^{0.45} \rho^{0.13} \mu^{0.025}$$

- Determine pump maximum output pressure from hp & unit analysis  
 Estimate actual efficiencies of pump and motor, Fig.'s 12-17 & 12-18
- Determine pipe purchase cost from Fig. 12-4  
 Determine fittings price from Fig. 14-4 (old 4th ed)  
 Determine valve purchase cost from Fig. 12-8 (flanged)  
 Determine pump purchase cost from Fig. 12-20  
 Determine magnesia insulation purchase cost from Fig. 12-12  
 Update with M&S equipment cost index
- Determine installation and insulation from Ch. 6 page 246 top paragraph info
- Forecast future M&S equipment cost index from handout figures

**Parameters:** Water density 62.4 lb./ft<sup>3</sup> 297 K water t 996 kg/m<sup>3</sup>  
 0.855 cP 0.000855 Pa s  
 Jan. 2002 1,102.5 M&S Jan. 2002 1,431.7 2<sup>nd</sup> qtr 2008  
 Jan. 1990 904.0 M&S Jan. 1990 for P&T 4th ed. Fittings cost  
 Installation 45 % of total installed cost for installation labor  
 Insulation 20 % of total installed cost for insulation material & labor  
 from page 246 1<sup>st</sup> paragraph, assume mid-range values

### Calculations:

convert to SI units for use of text figures  
 water delivery rate  $m_v =$  0.0174 m<sup>3</sup>/s 23.9 C water temperature  
 0.6 ft<sup>3</sup>/s velocity  
 eqn. 12-15 optimum diameter 0.120 m 4.7 inch diameter 1.52 meters/sec  
 select standard nominal pipe size, round up to **6** **6.065** inches **0.154** meters, actual ID 0.93 meters/sec

alt. round down to

**4 4.026**

**0.102**

2.11 meters/sec

**Answer a}**

check Reynolds Number for Turbulent flow,  $N_{Re} = D V \rho / \mu$  m m<sup>3</sup>/s/m<sup>2</sup> kg/m<sup>3</sup> / kg/m s

$N_{Re} = 167,081$  much > 2,100 thus Turbulent

Equivalent  $\Delta P_{PSI} = 10 \text{ hp} * 550 \text{ ft-lb/hp-sec} / m_v \text{ ft}^3/\text{sec} / 144 \text{ in}^2/\text{ft}^2$  429.7096 kPa from 10 hp \* 0.745W/hp / m<sup>3</sup>/s

m<sup>2</sup> kg / s<sup>3</sup> m<sup>3</sup>/s 62.3 psi lbf / in<sup>2</sup> 429.8306 kPa from psi \* 6.894

Pump capacity factor = m<sup>3</sup>/s \* kPa 7.46 m<sup>3</sup>/s x kPa

Alt. 4" pipe

Read pipe Fig. 12-4 pp 503	0.15 meter	\$30	per meter Sch.40 Carbon-steel welded pipe	0.1 m	\$18
Read fittings Fig. 14-4 copy	0.15 meter (in 1990)	\$90	per Tee Sch.40 Carbon-steel welded fitting	0.1 m	\$40
Read valves Fig. 12-8 pp 505	0.15 meter	\$1,100	per Gate valve flanged 1035 kPa carbon steel	0.1 m	\$750
Read pump Fig. 12-20 pp 518	7.46 m <sup>3</sup> /s x kPa	\$3,700	AVS horizontal, 150 psi		
Read insulation Fig. 12-12 pp 5	0.15 meter	\$18	per meter 85% magnesia 0.038m thick	0.1 m	\$15

Jan. 2002	length * cost/length	\$9,144			\$5,486
M&S update purchased cost	pipe	\$11,874	2nd qtr 2008	\$11.87 current \$/foot price	\$7.12 \$7,125
	fittings	\$5,701		\$142.54 current \$/tee price	\$63.35 \$2,534
	valves	\$5,714		\$1,428.45 current \$/valve price	\$973.95 \$3,896
	insulation	\$7,125		\$7.12 current \$/foot price	\$5.94 \$5,937
	pump	\$4,805		\$4,804.80 current \$/pump price	\$4,805

**Answer b}**

**\$35,200** purchased cost of pump + pipe equipment in 2nd qtr 2008

**\$24,300**

Cost to install pipe

Total Installed Cost = Purchased cost + 0.45 total installed  
\$ 64,000

TIC(1-0.45) = PC \$ 44,182

**Answer c}**

**\$ 64,000** installed cost of pump+pipe in 2nd qtr 2008

**\$ 44,200**

assume optimistic low projection of 1983-2003 year linear fit	18	units per year	1454.2	5 quarters into futu
\$65,000 low forecast of installed cost of pump+pipe				
assume pessimistic projection of last 2.5 year linear fit	160	units per year	1631.7	
\$72,900 high forecast of installed cost of pump+pipe				
80 forecast M&S index	3 <sup>rd</sup> qtr 2008	1,511.7	64 assumed units/yr increase	

**Answer d}**

**\$68,000** forecast installed cost of pump+pipe in 3rd qtr 2008 ± ~\$1,500 reasonable range

**\$47,000**

prepared by: D. C. Drown  
9/25/2008

## Supplemental Problem A-6 part II

Ch. 12 Materials Handling

**Goal:** Determine total installed cost of 3x5 pump & piping system

**Given:** Water pipe 275 gpm 75 F 1000 feet  
 delivery rate water temperature length 304.8 meter length  
 black carbon steel Insulation, 85% magnesia 1.5 inch thickness  
 Fittings 40 Valves 4  
 Pump 10 hp centrifugal  
 Motor AC enclosed 3-phase 1800 rpm

**Approach:** Same as Part I except replace the single pump with 5 smaller 40% pumps  
 Design for 3 pumps each handling 40% of load and 2 on stand-by  
 Use 40% of pump capacity factor for each of the 5 pumps  
 Determine pump purchase cost from Fig. 12-20

**Parameters:** Water density 62.4 lb./ft<sup>3</sup> 297 K water temp 996 kg/m<sup>3</sup>  
 0.855 cP 0.000855 Pa s  
 Jan. 2002 1,102.5 M&S Jan. 2002 1,431.7 2<sup>nd</sup> qtr 2008  
 Jan. 1990 904.0 M&S Jan. 1990 for P&T 4th ed. Fittings cost  
 Installation 45 % of total installed cost for installation labor  
 Insulation 20 % of total installed cost for insulation material & labor  
 from page 246 1<sup>st</sup> paragraph, assume mid-range values

### Calculations:

convert to SI units for use of text figures  
 water delivery rate  $m_v = 0.0174 \text{ m}^3/\text{s}$  23.9 C water temperature 0.6 ft<sup>3</sup>/s velocity  
 eqn. 12-15 optimum diameter 0.120 m 4.7 inch diamete actual ID 1.52 meters/sec  
 select standard nominal pipe size, round up to 6.0 inches 0.152 meters 0.154 0.93 meters/sec  
 select standard nominal pipe size, round down to 4.0 inches 0.102 meters 0.102 2.11 meters/sec

### Answer a}

check Reynolds Number for Turbulent flow,  $N_{Re} = D V \rho / \mu$  m m<sup>3</sup>/s/m<sup>2</sup> kg/m<sup>3</sup> / kg/m s

$N_{Re} = 167,081$  much > 2,100 thus Turbulent 251,701

Equivalent $\Delta P_{PSI} = 10 \text{ hp} * 550 \text{ ft-lb/hp-sec} / m_v \text{ ft}^3/\text{sec} / 144 \text{ in}^2/\text{ft}^2$		429.7096 kPa	from 10 hp * 0.745W/hp / m3/s			
$m^2 \text{ kg} / s^3 \text{ m}^3/s$	62.3	psi	lbf / in <sup>2</sup>	429.8306 kPa		
Pump capacity factor = $m^3/s * kPa$	2.98	$m^3/s * kPa$		from psi * 6.894		
				nominal 4"		
				0.10		
Read pipe Fig. 12-4 pp 503	0.15	meter	\$30	per meter Sch.40 Carbon-steel welded pipe	\$18	
Read fittings Fig. 14-4 copy	0.15	meter (in 1990)	\$90	per Tee Sch.40 Carbon-steel welded fitting	\$40	
Read valves Fig. 12-8 pp 505	0.15	meter	\$1,100	per Gate valve flanged 1035 kPa carbon steel	\$750	
Read pump Fig. 12-20 pp 518	2.98	$m^3/s * kPa$	\$2,800	AVS horizontal, 150 psi		
Read insulation Fig. 12-12 pp 5	0.15	meter	\$18	per meter 85% magnesia 0.038m thick	\$15	
Jan. 2002		length * cost/length		\$9,144	\$7,125	
M&S update purchased cost		pipe	\$11,874	2nd qtr 2008	\$11.87 current \$/foot price	\$7.12
		fittings	\$5,701		\$142.54 current \$/tee price	\$63.35
		valves	\$5,714		\$1,428.45 current \$/valve price	\$973.95
		insulation	\$7,125		\$7.12 current \$/foot price	\$5.94
		pumps	\$18,180		\$3,636.06 current \$/pump price	

**Answer b}** **\$48,600** purchased cost of pump+pipe equipment in 2nd qtr 2008 \$33,500

Cost to install pipe

Total Installed Cost = Purchased cost + 0.45 total installed  
 \$ 88,364 TIC(1-0.45) = PC \$ 60,909

**Answer c}** **\$88,400** installed cost of 3x5 pumps+pipe in 2nd qtr 2008 \$60,900

\$24,400 additional investment for redundant 3x5 pumps compared to single pump  
 38% increase in capital cost, but system could easily supply 20% more (50 gpm) water in an emergency

Note: neglected added costs for more valves and fittings to manifold the 5 pumps together in parallel  
 \$23,369 need at least 8 more valves and 10 more fittings with 4" manifold \$15,318

**Answer c}** **\$112,000** installed cost of 3x5 pumps+pipe in 2nd qtr 2008 **\$104,000** \$ 76,000

prepared by: D. C. Drown  
 9/25/2008